

Effect of Suction and Injection on Unsteady Solute Transfer in a Micropolar Fluid under the Influence of Magnetic Field

Venkataswamy K V, Indira Ramarao, Jagadeesha S

Department of Mathematics,
Nitte Meenakshi Institute of Technology, Bangalore, India.

Abstract

A micropolar fluid is flowing in a channel with suction and injection under the influence of magnetic field. An unsteady mass transfer is considered under these conditions. The governing equations arising are solved analytically and solutions obtained are graphically depicted. It is seen that the effect of micropolar fluid is to slow down convection, hence facilitating retention of solute at the targeted region.

AMS Subject Classification: 76Rxx

Keywords: Suction, injection, micropolar fluid, magnetic field, solute transfer.

1. Introduction

Blood is the main source of delivering nutrients, drugs and oxygen to the tissue removal of wastes. Blood consists of particulate matter which cause spinning and micro rotation giving rise to an angular velocity. Blood behaves like Newtonian as well as non-Newtonian depending on circumstances. [1] have developed

a model presenting theoretical study of slow of Bingham fluid in porous media. A theoretical study of blood flow in micro circulation has been considered by [2] and [3], in which blood is considered as Casson fluid.

[4] have considered couple stress fluid through stenotic blood vessels. [5] have studied peristaltic flow of couple stress fluid. [6] and [7] have studied the blood flow through a stenosed catheterised artery.

In case of dialysis, flow through capillaries in tissue region involve permeable wall. [8] have studied pulsatile flow through circular tubes with varying cross section. [9] have analysed the second grade fluid flowing in a channel with effects of suction and injection and side walls. [10] have considered flow past porous boundary and got the exact solution. [11] studied the effect of couple stress on flow in a doubly connected region.

In the present study, a convective diffusive mass transfer of an injected tracer in a micropolar fluid is considered flowing through a rectangular channel with suction and injection under the influence of magnetic field.

2. Mathematical Formulation

The physical configuration shows a rectangular channel with suction and injection under the influence of magnetic field.

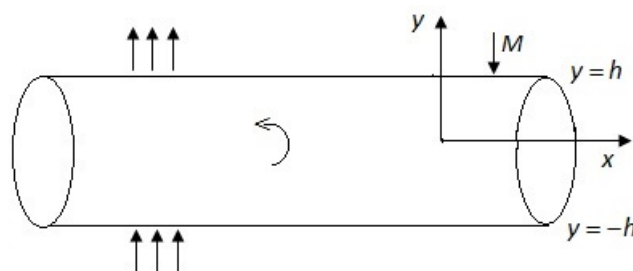


Figure 1: Physical configuration

Under the assumption of a fully developed flow, the governing equation for a micropolar fluid is given by,

$$\rho \left[v \frac{\partial u}{\partial y} \right] = -\frac{\partial p}{\partial x} + (\mu + \kappa) \frac{\partial^2 u}{\partial y^2} + \kappa \frac{\partial N}{\partial y}, \quad (1)$$

$$\left[\mu + \frac{1}{2} \kappa \right] j \frac{\partial^2 N}{\partial y^2} - \kappa \left[2N + \frac{\partial u}{\partial y} \right], \quad (2)$$

where u , N , κ , j and μ are the axial velocity, angular velocity, vortex viscosity, microinertia and dynamic viscosity respectively.

The species equation is given by,

$$\frac{\partial c}{\partial t} + u \frac{\partial c}{\partial x} = D \left[\frac{\partial^2 c}{\partial x^2} + \frac{\partial^2 c}{\partial y^2} \right], \quad (3)$$

subject to boundary conditions,

On velocity:

$$\left. \begin{aligned} u &= -u_0 \text{ at } y = h \\ u &= u_0 \text{ at } y = -h \\ N &= 0 \text{ at } y = \pm h \end{aligned} \right\}, \quad (4)$$

On concentration:

$$\left. \begin{aligned} c(0, x, y) &= c_0 \\ D \frac{\partial c}{\partial y} &= -kc \text{ at } y = h \\ D \frac{\partial c}{\partial y} &= kc \text{ at } y = -h \\ c(t, \infty, y) &= \frac{\partial c}{\partial y}(t, \infty, y) = 0 \end{aligned} \right\}. \quad (5)$$

Non-dimensionalisation is carried out using the parameters,

$$\left. \begin{aligned} (u^*, v^*, N^*) &= \frac{(u, v, Nh)}{u_0}, \quad y^* = \frac{y}{h}, \quad t^* = \frac{Dt}{h^2}, \\ x^* &= \frac{Dx}{h^2 u_0}, \quad \theta = \frac{c}{c_0}, \quad Pe = \frac{hu_0}{D}, \quad \beta = \frac{kh}{D}. \end{aligned} \right\} \quad (6)$$

and neglecting the asterisks(*) for simplicity we get,

$$Re \frac{\partial u}{\partial y} v = -P + (1 + R) \frac{\partial^2 u}{\partial y^2} + R \frac{\partial N}{\partial y}, \quad (7)$$

$$\frac{\partial^2 N}{\partial y^2} - \frac{RB}{1 + \frac{1}{2}R} \left[2N + \frac{\partial u}{\partial y} \right] = 0, \quad (8)$$

$$\frac{\partial \theta}{\partial t} + u \frac{\partial \theta}{\partial x} = \frac{1}{Pe^2} \frac{\partial^2 \theta}{\partial x^2} + \frac{\partial^2 \theta}{\partial y^2}, \quad (9)$$

subject to boundary conditions,

$$\left. \begin{aligned} u &= -1 \text{ at } y = 1 \\ u &= 1 \text{ at } y = -1 \\ N &= 0 \text{ at } y = \pm 1 \end{aligned} \right\}, \quad (10)$$

and

$$\left. \begin{aligned} \theta(0, x, y) &= 1 \\ \frac{\partial \theta}{\partial y} &= -\beta \theta \text{ at } y = 1 \\ \frac{\partial \theta}{\partial y} &= \beta \theta \text{ at } y = -1 \\ \theta(t, \infty, y) &= \frac{\partial \theta}{\partial y}(t, \infty, y) = 0 \end{aligned} \right\}. \quad (11)$$

Solving analytically for velocity and angular velocity, using boundary conditions given in (10) we get,

$$\begin{aligned} N &= \frac{P}{c} e^{(\frac{a}{3} + \alpha)y} \left[\frac{\cosh(\frac{a}{3} - \alpha)}{\cos \beta} \cos \beta y + \frac{\sinh(\frac{a}{3} - \alpha)}{\sin \beta} \sin \beta y \right] \\ &+ c_1 e^{\frac{a}{3}y} \left[e^{k_1 y} - e^{\alpha y} \left\{ \frac{\cosh(k_1 - \alpha) \cos \beta \cos \beta y}{\sin \beta} \right. \right. \\ &\left. \left. + \frac{\sinh(\frac{a}{3} - \alpha) \sin \beta y}{\sin \beta} \right\} \right], \end{aligned} \quad (12)$$

and

$$\begin{aligned} u &= -\frac{P}{c} \left[\frac{c_1 \Gamma_3 e^{(\frac{a}{3} + k_1)y}}{\frac{a}{3} + k_1} - \frac{c_1 e^{(\frac{a}{3} + \alpha)y}}{g^2 + \beta^2} \right. \\ &\left. \{ \Gamma_4 (g \cos \beta y + \beta \sin \beta y) - \Gamma_5 (g \sin \beta y - \beta \cos \beta y) \} \right. \\ &\left. + c_2 - \frac{e^{(\frac{a}{3} + \alpha)y}}{g^2 + \beta^2} \right. \\ &\left. \{ \Gamma_1 (g \cos \beta y + \beta \sin \beta y) + \Gamma_2 (g \sin \beta y - \beta \cos \beta y) \} \right]. \end{aligned} \quad (13)$$

The constants are listed in the appendix.

To solve the species equation the method is used by [12] is modified and adopted. Averaging θ in the region between -1 to 1 and using the dispersion model,

$$\theta = \sum_{k=0}^{\infty} f_k(t, y) \frac{\partial^k \theta_m}{\partial x^k},$$

and

$$\frac{\partial \theta_m}{\partial t} = \sum_{j=0}^{\infty} K_j \frac{\partial^j \theta_m}{\partial x^j}. \quad (14)$$

Using the equation (16) in the equation (9) and simplifying, we get

$$\frac{\partial f_k}{\partial t} = \frac{\delta_{k2}}{Pe^2} f_{k-2} + \frac{\partial^2 f_k}{\partial y^2} - u f_{k-1} - \sum_{k=0}^{\infty} \sum_{j=0}^k K_j f_{k-j}. \quad (15)$$

Solving for f_0 and f_1 , the resulting equations and using the condition $\int_{-1}^1 f_0 dy = 1$, $\int_{-1}^1 f_k dy = 0$ for $k = 1, 2, 3, \dots$ we obtain

$$f_0 = \frac{\sum A_i e^{-\mu_i^2 t} \cos \mu_i y}{\sum \frac{A_i}{\mu_i} e^{-\mu_i^2 t} \sin \mu_i y}, \quad (16)$$

and

$$K_0(t) = -\frac{\sum A_n \mu_n e^{-\mu_n^2 t} \sin \mu_n y}{\sum \frac{A_n}{\mu_n} e^{-\mu_n^2 t} \sin \mu_n y} \quad (17)$$

For large time as $t \rightarrow \infty$ we get,

$$f_0 = \frac{\mu_0}{\sin \mu_0},$$

and

$$K_0 = -\mu_0^2. \quad (18)$$

Similarly for solving for f_1 and f_2 using,

$$\frac{\partial f_k}{\partial y} = \begin{cases} -\beta f_k & \text{at } y = 1 \\ \beta f_k & \text{at } y = -1 \end{cases}, \quad (19)$$

we can find,

$$K_1(t) = \frac{I_1(0,0)}{1 + \frac{\sin 2\mu_0}{2\mu_0}},$$

and

$$K_2(t) = \frac{1}{Pe^2} - \frac{\sin \mu_0}{\mu_0 \left(1 + \frac{\sin 2\mu_0}{2\mu_0}\right)} \sum B_{j,1} I(j,0), \quad (20)$$

where $I(j,l) = \int_{-1}^1 u \cos \mu_j y \cos \mu_l y dy$ for $j \neq l$ and

$$I(j,l) = \int_{-1}^1 u \cos^2 \mu_j y dy \text{ for } j = l.$$

The mean concentration is obtained by solving,

$$\frac{\partial \theta_m}{\partial t} = K_0(t) \theta_m + K_1(t) \frac{\partial \theta_m}{\partial x} + K_2(t) \frac{\partial^2 \theta_m}{\partial x^2}, \quad (21)$$

subject to boundary conditions,

$$\theta_m(0,x) = \begin{cases} 1 & \text{if } |x| \leq L \\ 0 & \text{if } |x| > L \end{cases}, \quad (22)$$

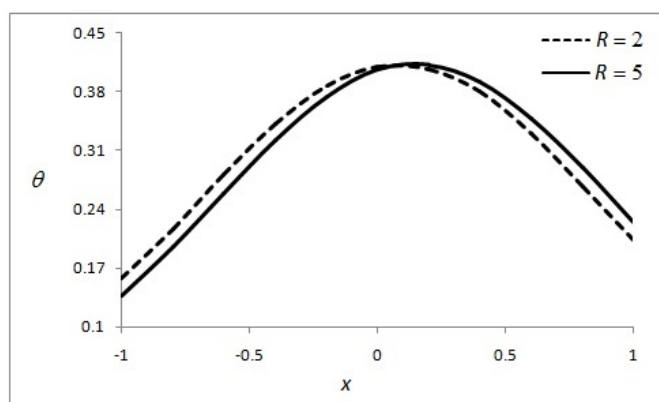


Figure 2: Concentration profile for different values of microrotation parameter at $t = 0.3$

we get

$$\theta_m = \frac{1}{\sqrt{2M}} \left[\zeta - \frac{\xi^2}{4M} \right], \quad (23)$$

where $M = K_0 t$, $\zeta = x + K_1 t$ and $\xi = K_2 t$.

3. Numerical Results

In the present study, the species transport equation governing convective diffusive mass transfer of traces introduced in a micropolar fluid flowing in a rectangular channel with effects of suction and injection is studied. Using analytical methods concentration is depicted graphically for different parameters arising in the study corresponding to the values which taken from the available literature.

Figure 2 shows the effect of microrotation which is negligible for long time but increases with increasing microrotation parameter. But in axial direction the effect is considerable for a fixed time. At $t = 0.3$ we see that initially the concentration is higher for microrotation parameter $R = 2$ compared to $R = 5$.

In figure 3 we can observe the intersection of curves at $X = 0$ and from 0 to 1, the curve of $R = 5$ is showing higher value. As the fluid flows from $X = -1$ to $X = 1$ due to convection, the effect of microrotation gets reversed.

Figure 4 shows the effect of microrotaion against time. In general, the effect of micropolar fluid is to slow down the convection of drug during the process. As the suction velocity decreases, the convection along axis increases and hence concentration increases axially.

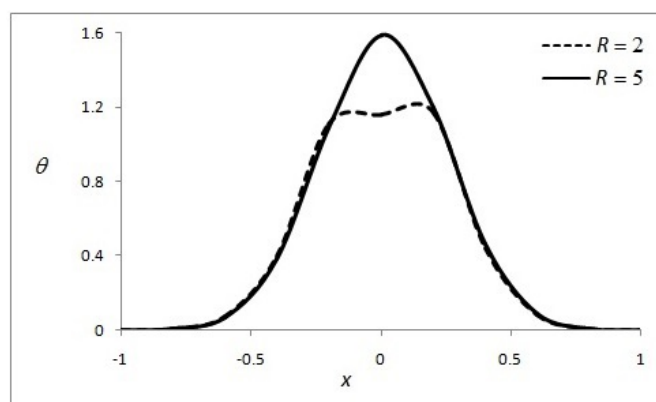


Figure 3: Concentration profile for different values of microrotation parameter at $t = 0.03$

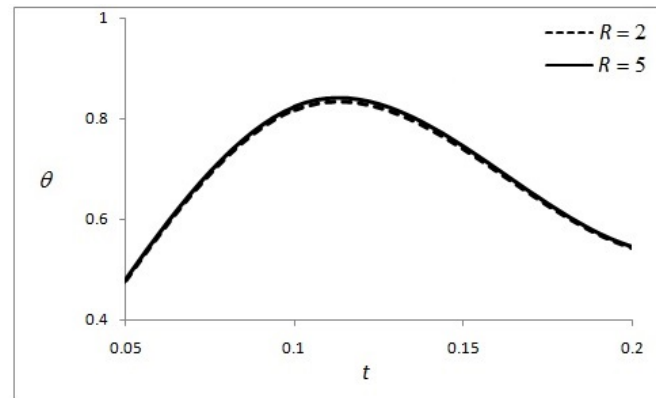


Figure 4: Concentration profile vs. time for different values of microrotation parameter

4. Conclusions

The effect of micropolar fluid under the influence of magnetic field in presence of suction and injection at walls on convective diffusive mass transfer is studied. Effect of micropolar fluid is more visible in axial direction. As time progresses, the effect of microrotation is negligible. Effect of suction is to reduce the convection.

Acknowledgement

The authors thank the management of Nitte Meenakshi Institute of technology, Yelahanka, Bangalore - 560064 for their support in carrying out this work.

References

- [1] Wu, Y. S., Pruess, K., Witherspoon, P. A., 1990, "Flow and displacement of Bingham non-Newtonian fluids in porous media", LBL-28340, pp. 1 - 31.
- [2] Schmid-Schonebein, G. W., 1988, "A theory of blood flow in skeletal muscle", Trans. ASME, J. Biomed. Engg., 110(1), pp. 20 - 26.
- [3] Ashish, T., and Satyendra, S. C., G. W., 2018, "Effect of Varying Viscosity on Two-Fluid Model of Blood Flow through Constricted Blood Vessels: A Comparative Study", Cardiovascular Engineering and Technology, pp. 1 - 18.
- [4] Srivastava, V. P., and Saxena, M., 1994, "Two layered model of casson fluid flow through stenotic blood vessels; Applications to cardiovascular system", J. Biomech. Engg., Volume 27, Issue 7, pp. 921 - 928.
- [5] Mecheimer, K. S., and Abdelmabound, Y., 2008, "Peristaltic flow of a couple stress fluid in an annulus: Application of an endoscope", Physica A: Statistical Mechanics, Vol 387, Issue 11, pp. 2403 - 2415.
- [6] Srivastava, V. P., and Rastogi, R., 2010, "Blood flow through a stenosed catheterized artery: Effects of hematocrit and stenosis shape", Comp. and Math. wit Appl., Vol 59, Issue 4, pp. 1377 - 1385.
- [7] Sankar, D. S., and Yatim, Y., 2012, "Comparative analysis of mathematical models for blood flow in tapered constricted arteries", Abstract and Applied Analysis, Article ID 235960, pp. 1 - 34.
- [8] Schneck, D. J., and Simon O., 1975, "Pulsatile blood flow in a channel of small exponential divergence: The linear approximation for mean Reynolds number", J. fluids Engg., Vol 97, Issue 3, pp. 353 - 360.
- [9] Erdogan, M. E., and Imrak, C. E., 2007, "The effects of the sidewalls on the flow of a second grade fluid in ducts with suction and injection", I. J. of Non-linear Mech., Vol 42, pp. 765 - 772.
- [10] Griffith, A., and Meredith, F., 1936, "The possible improvement in aircraft performance due to the use of boundary layer suction", Roy. Aircraft Establishment Report, No. E3501, pp. 12.
- [11] Indira, R., Venkatachalappa, M., and Siddheshwar, P. G., 2008, "Flow of couple stress fluid between two eccentric cylinders", IJMSEA, Vol 2, No. IV, pp. 253 - 261.
- [12] Sankarasubramanian, R., and Gill, W. N., 1973, "Taylor diffusion in laminar flow in an eccentric annulus", Proceedings of the Royal Society of London, A, 333, IJMSEA, pp. 115 - 132.

Appendix

$$c_1 = \frac{1}{g^2 + \beta^2} \left[\frac{2c + \frac{2l_1}{g^2 + \beta^2}}{l_2 - l_3} \right],$$

$$c_2 = c - \frac{e^g}{g^2 + \beta^2} l_4 + c_1 l_5,$$

$$l_1 = (\Gamma_3 g - \Gamma_2 \beta) \cos \beta \sinh(g) + (\Gamma_2 g + \Gamma_3 \beta) \sin \beta \cosh(g),$$

$$l_2 = \frac{2\Gamma_1}{\frac{a}{3} + k_1} \sinh\left(\frac{a}{3} + k_1\right),$$

$$l_3 = \frac{2}{g^2 + \beta^2} (\Gamma_4 g - \Gamma_2 \beta) \cos \beta \sinh(g) + (\Gamma_2 g + \Gamma_4 \beta) \sin \beta \cosh(g),$$

$$l_4 = \Gamma_1 (g \cos \beta + \beta \sin \beta) + \Gamma_2 (g \sin \beta - \beta \cos \beta),$$

$$l_5 = \frac{e^{\frac{a}{3} + k_1}}{\frac{a}{3} + k_1} - \frac{e^g}{g^2 + \beta^2} [\Gamma_4 (g \cos \beta + \beta \sin \beta) - \Gamma_5 (g \sin \beta - \beta \cos \beta)],$$

$$\Gamma_1 = \frac{1 + \frac{R}{2}}{RB} \left[\frac{\cosh\left(\frac{a}{3} - \alpha\right)}{\cos \beta} (g^2 - \beta^2) + \frac{\sinh\left(\frac{a}{3} - \alpha\right)}{\sin \beta} (2g\beta) \right] + \frac{2\cosh\left(\frac{a}{3} - \alpha\right)}{\cos \beta},$$

$$\Gamma_2 = \frac{1 + \frac{R}{2}}{RB} \left[\frac{\cosh\left(\frac{a}{3} - \alpha\right)}{\cos \beta} (-2g\beta) + \frac{\sinh\left(\frac{a}{3} - \alpha\right)}{\sin \beta} (g^2 + \beta^2) \right] + \frac{\sinh\left(\frac{a}{3} - \alpha\right)}{\sin \beta},$$

$$\Gamma_3 = \frac{1 + \frac{R}{2}}{RB} \left[\frac{a}{3} + k_1 \right]^2 - 2,$$

$$\Gamma_4 = \frac{1 + \frac{R}{2}}{RB} \left[\frac{\cosh(k_1 - \alpha)}{\cos \beta} (g^2 - \beta^2) + \frac{\sinh(k_1 - \alpha)}{\sin \beta} (2g\beta) \right] + \frac{2\cosh(k_1 - \alpha)}{\cos \beta},$$

$$\Gamma_5 = \frac{1 + \frac{R}{2}}{RB} \left[\frac{\cosh(k_1 - \alpha)}{\cos \beta} (2g\beta) - \frac{\sinh(k_1 - \alpha)}{\sin \beta} (g^2 + \beta^2) \right] + \frac{2\sinh(k_1 - \alpha)}{\sin \beta},$$

$$g = \frac{a}{3} + \alpha, \quad \beta = -\frac{\sqrt{3} \left[2^{\frac{2}{3}} (a^2 + 3b) - \alpha_0^{\frac{2}{3}} \right]}{[2^4 \alpha_0]^{\frac{1}{3}}}, \quad \alpha = -\frac{\left[2^{\frac{2}{3}} (a^2 + 3b) + \alpha_0^{\frac{2}{3}} \right]}{[2^4 \alpha_0]^{\frac{1}{3}}},$$

$$k_1 = \frac{\left[2^{\frac{2}{3}} (a^2 + 3b) + \alpha_0^{\frac{2}{3}} \right]}{[2\alpha_0]^{\frac{1}{3}}},$$

$$\alpha_0 = 2a^3 + 9ab - 27c + 3\sqrt{81c^2 - 24abc - 12a^3c - 12b^3 - 3a^2b^2},$$

$$a = \frac{vRe}{1 + R}, \quad b = \frac{RB(2 + R)}{(1 + R) \left(1 + \frac{R}{2} \right)}, \quad c = \frac{2vReRB}{(1 + R) \left(1 + \frac{R}{2} \right)}.$$